

# Catalytic materials for plasma-based VOC removal

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# Outline



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- **Why use plasma + catalyst?**
- **Reactor configuration**
- **Technology of coating with catalyst**
- **Some performance results**
- **Summary**



# Why use plasma + catalyst?



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## In the plasma system with no catalyst;

- Air + hazardous impurities passed through a plasma discharge
- Bombardment of molecules by electrons and ions.
- Formation of ozone, atomic oxygen, hydroxyl groups, excited molecules and atoms
- Oxidation of VOCs to CO<sub>2</sub> and H<sub>2</sub>O



# Characteristics



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- **Not always complete decomposition of VOCs to CO<sub>2</sub> and H<sub>2</sub>O at acceptable discharge energies especially if VOC levels are high**
- **Residual ozone from outlet which must be removed**
  - needs a removal stage after the plasma stage
- **Can incorporate a catalyst in the system to improve decomposition and remove hazardous byproducts**
- **Standard catalysts need a high temperature**
- **Use an activated catalyst**



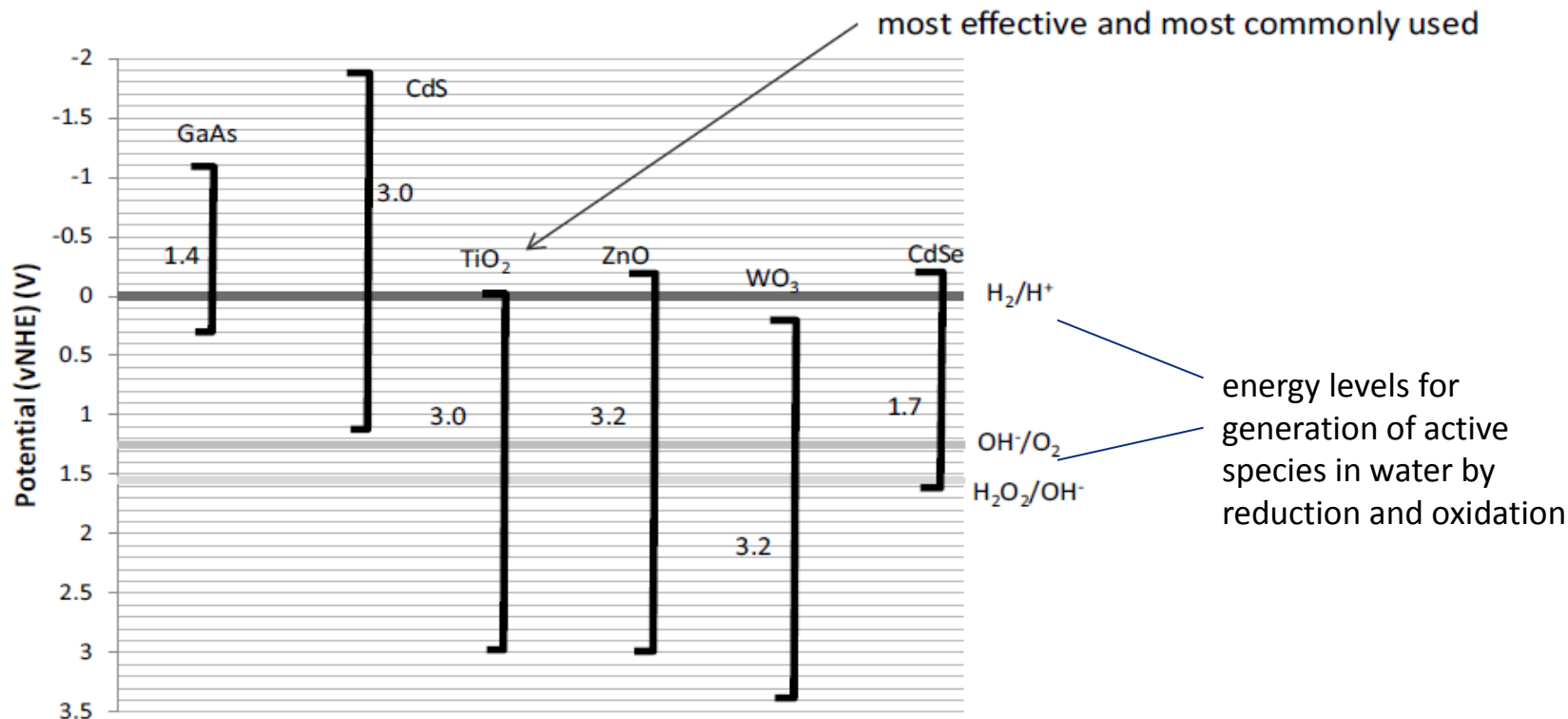


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# Photocatalysts

- Semiconductors are effective photocatalysts
- Need photoactivation by appropriate wavelengths
- Use plasma radiation to activate catalyst – don't need high temperatures to activate



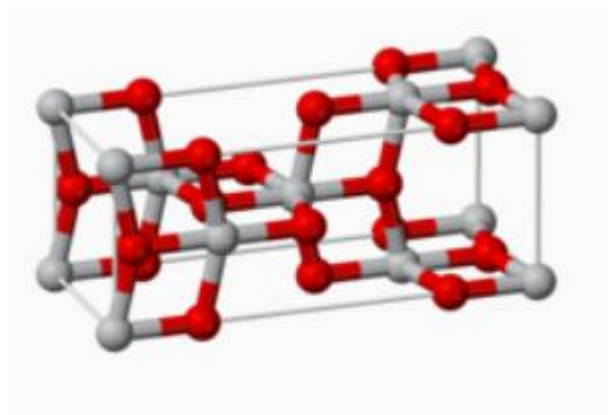
# Titanium dioxide



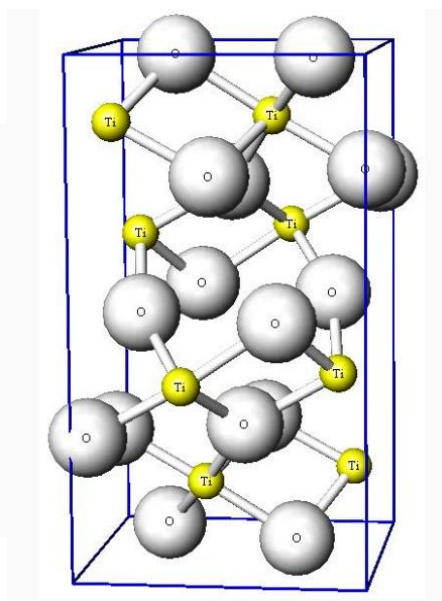
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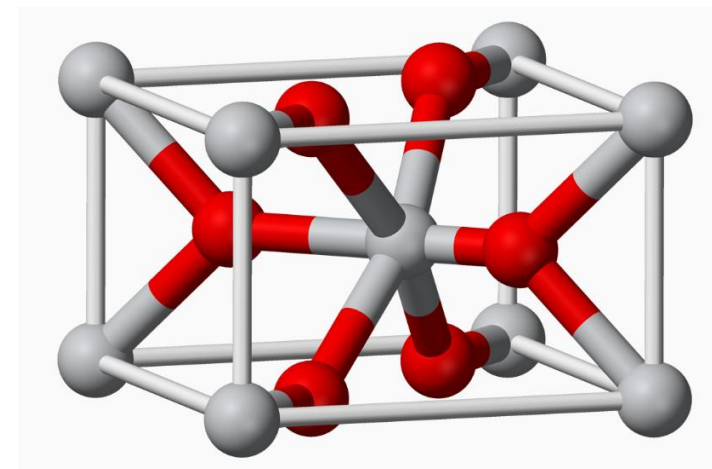
## 3 crystal phases



**Anatase**  
energy gap 3.2 eV  
stable at low temperature



**Brookite**  
energy gap 3.3 eV



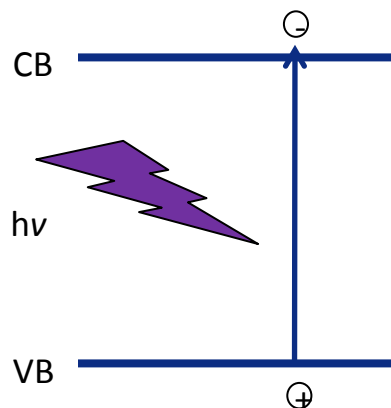
**Rutile**  
energy gap 3.0 eV  
stable at higher temperature



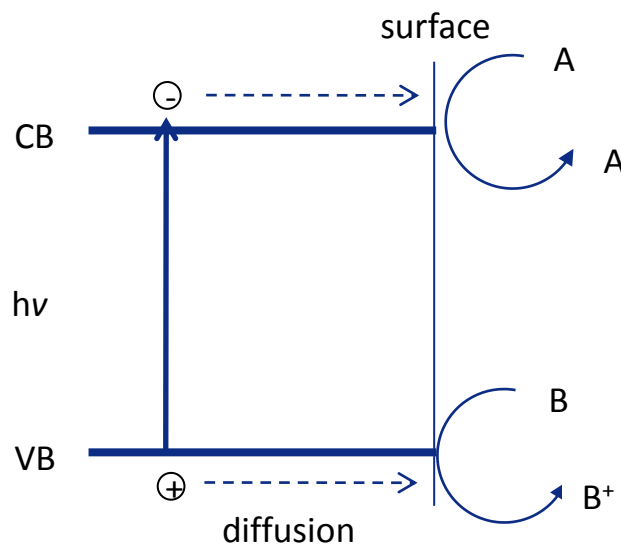
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# Mechanism of photocatalysis



Electrons and holes generated inside the catalyst must get to the surface so that they can cause a reaction.



Electrons and holes must diffuse to the surface in order to act on adsorbed species

Needs light with energy greater than bandgap to activate the catalyst  
– for  $\text{TiO}_2$  use UV light from the plasma

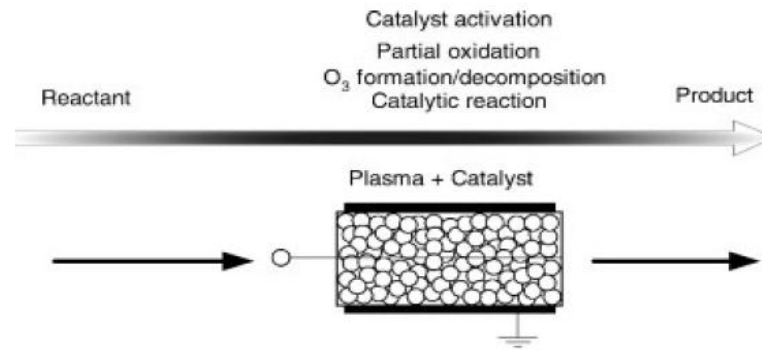


# Single-Stage Plasma Catalysis



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- **Combination of gas phase and surface reactions**
- **Reactions take place simultaneously**
- **Complicated reactions**
- **Maximises interaction of catalyst with plasma**
- **Can utilise short-lived plasma species to interact with the catalyst**



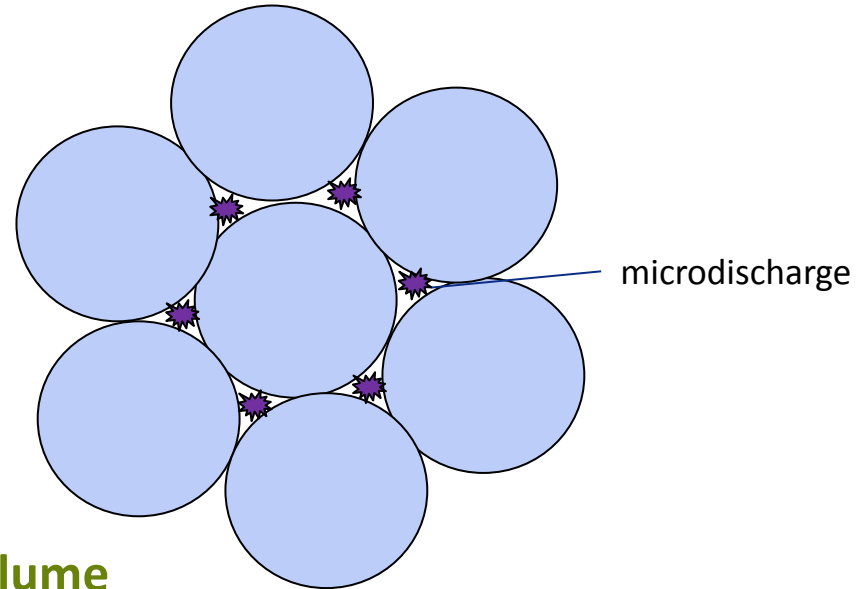
# Discharge enhancement



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- With single stage plasma, microdischarges can be generated inside pores or gaps between particles



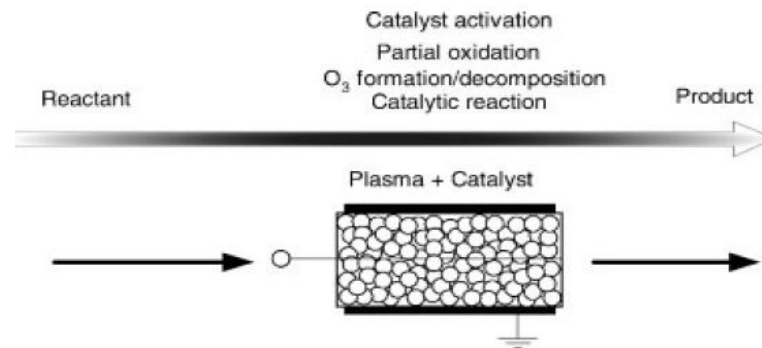
- More discharge energy per unit volume
- Higher mean energy density
- Electrical properties of particles are important



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# Packed bed structure



To maximise the surface area of the catalyst, it can be in

- pellet form, homogeneous or coated
- coated fibres

Our solution is to use porous materials with small pore size to maximise surface area

- how to coat internal surfaces of the pores?

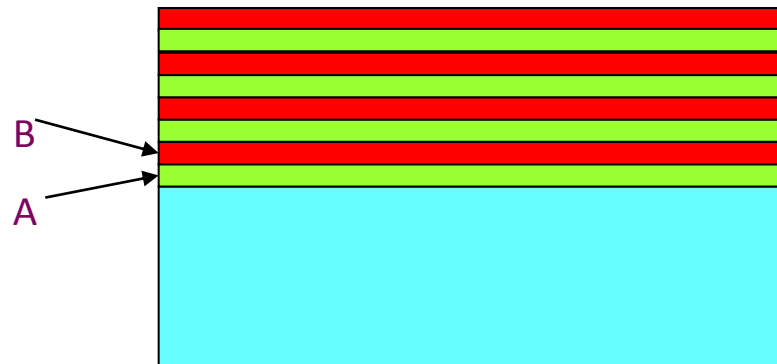
# Atomic Layer Deposition (ALD)



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- Materials are built up one atomic layer at a time.
- For example, a compound AB is built up of alternate layers of A and B one atomic layer thick at a time.
- Extremely conformal coating
- Can coat inside porous structures – if pores are bigger than precursor molecules

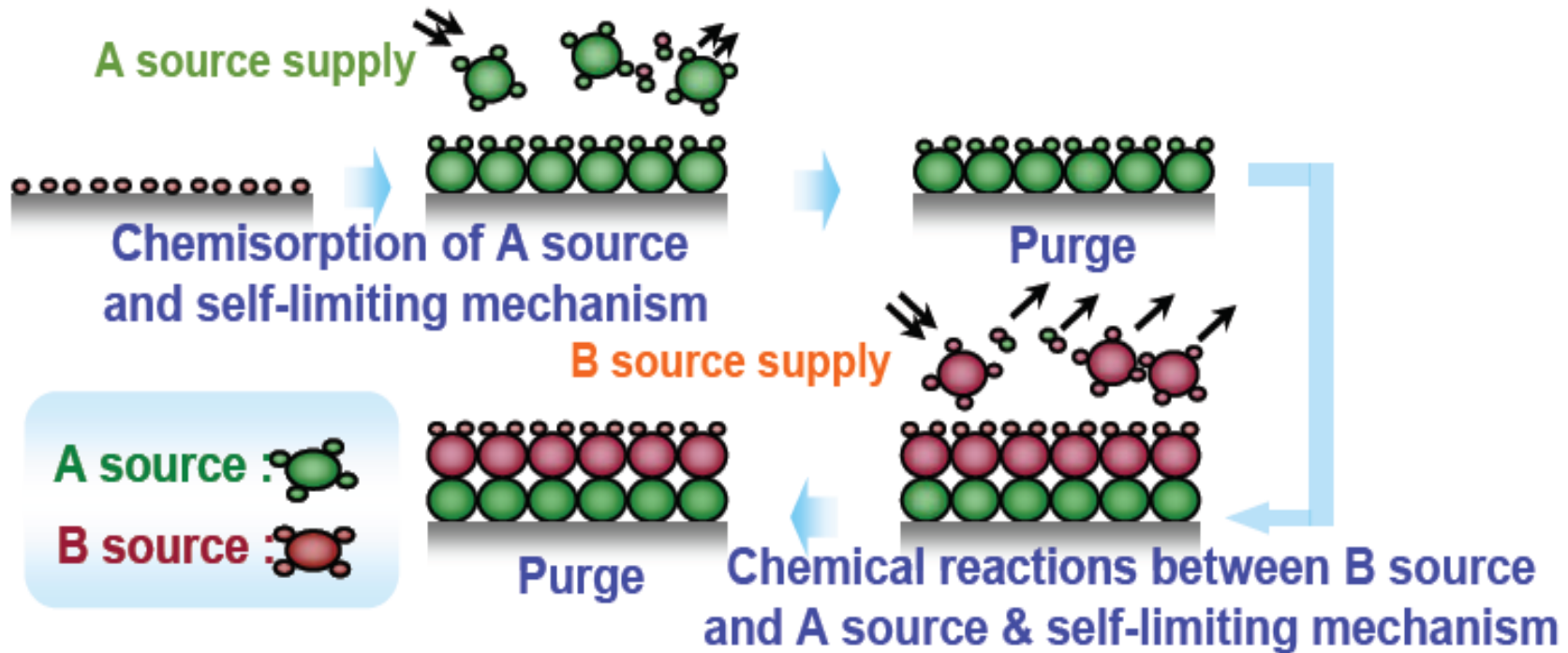


# ALD process cycle



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Repeat as many times as required



# Characteristics of ALD



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- **Chemical vapour deposition process**
- **Film thickness sub-nm to several hundred nm**
- **Extreme control over deposition – thickness controlled 'digitally',  
— depends on number of deposition cycles**
- **Complete conformality, even on complex shapes, within pores and on nanoparticles**
- **Can change the composition from layer to layer**



# ALD process for TiO<sub>2</sub>



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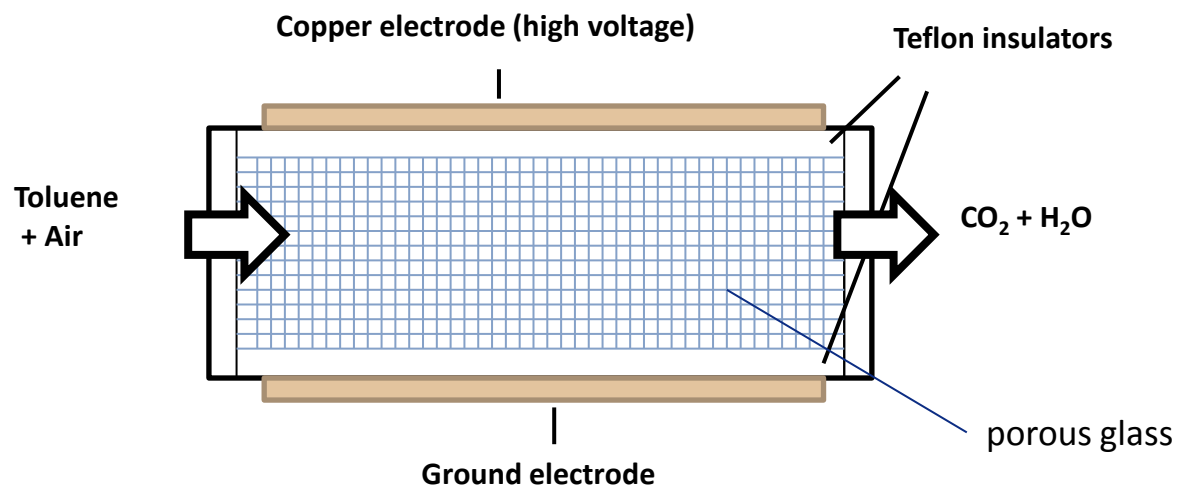
- Precursors TiCl<sub>4</sub> and H<sub>2</sub>O
  - both have a high enough vapour pressure at room temperature
- Reaction temperature 300°C
  - gives mainly anatase material

Beneq TFS 500 reactor



# Plasma reactor

- **Dielectric barrier discharge reactor**



- **Single stage reactor – plasma and catalyst in the same chamber**
- **Discharge gap with porous glass filling**
- **Pores coated by ALD**

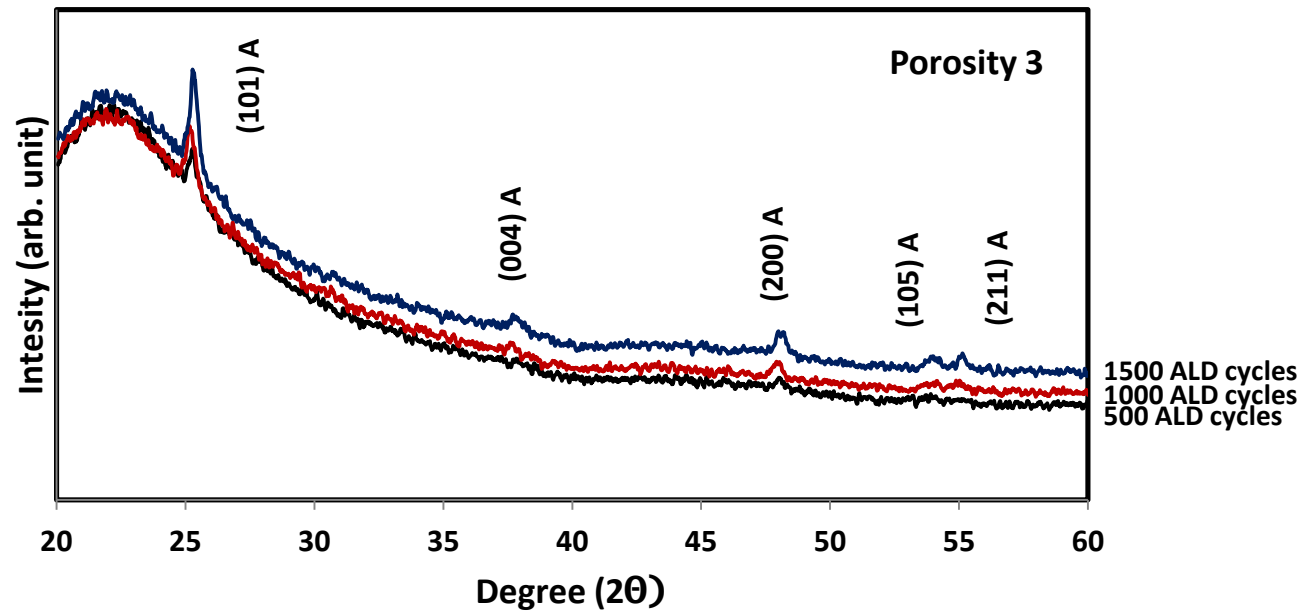
# Film structure



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## XRD analysis

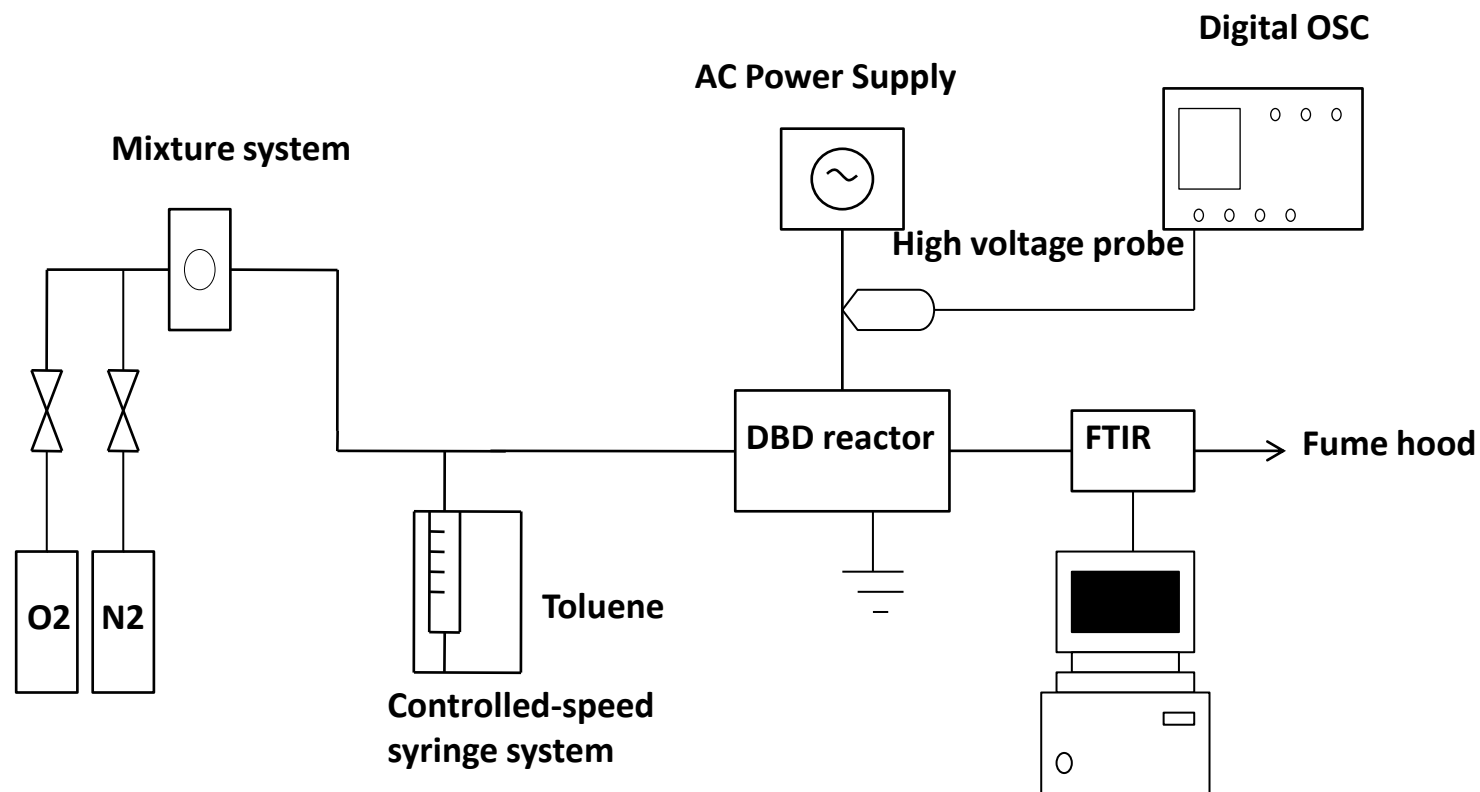


anatase structure





# Experimental set-up for measuring toluene degradation



# Efficiency of removal of VOCs



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- **Carbon balance**

$$\text{Carbon balance (\%)} = \frac{[CO_2] + [CO]}{n([VOC]_0 - [VOC])} \times 100$$

$n$  = no. of C atoms in VOC molecule  
 $[VOC]_0$  is input concentration of VOC molecules

- **CO<sub>2</sub> selectivity**

$$s_{CO_2} (\%) = \frac{[CO_2]}{[CO_2] + [CO]} \times 100$$

- **Specific input energy (SIE)**

$$SIE = \frac{P_{dis}}{Q_f} = \frac{\text{discharge power (W)}}{\text{gas flow rate (l/s)}} [J / l]$$



# Properties of porous glass



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## Catalyst support: borosilicate porous glass

- porosity #2, pore size 40 – 100  $\mu\text{m}$
- porosity #3, pore size 16 – 40  $\mu\text{m}$

## Inner surface (BET):

- porosity #2: 0,130  $\text{m}^2/\text{g}$
- porosity #3: 0,350  $\text{m}^2/\text{g}$

## TiO<sub>2</sub> film thickness:

500 cycles ~ 40 nm

1000 cycles ~ 80 nm

1500 cycles ~ 120 nm

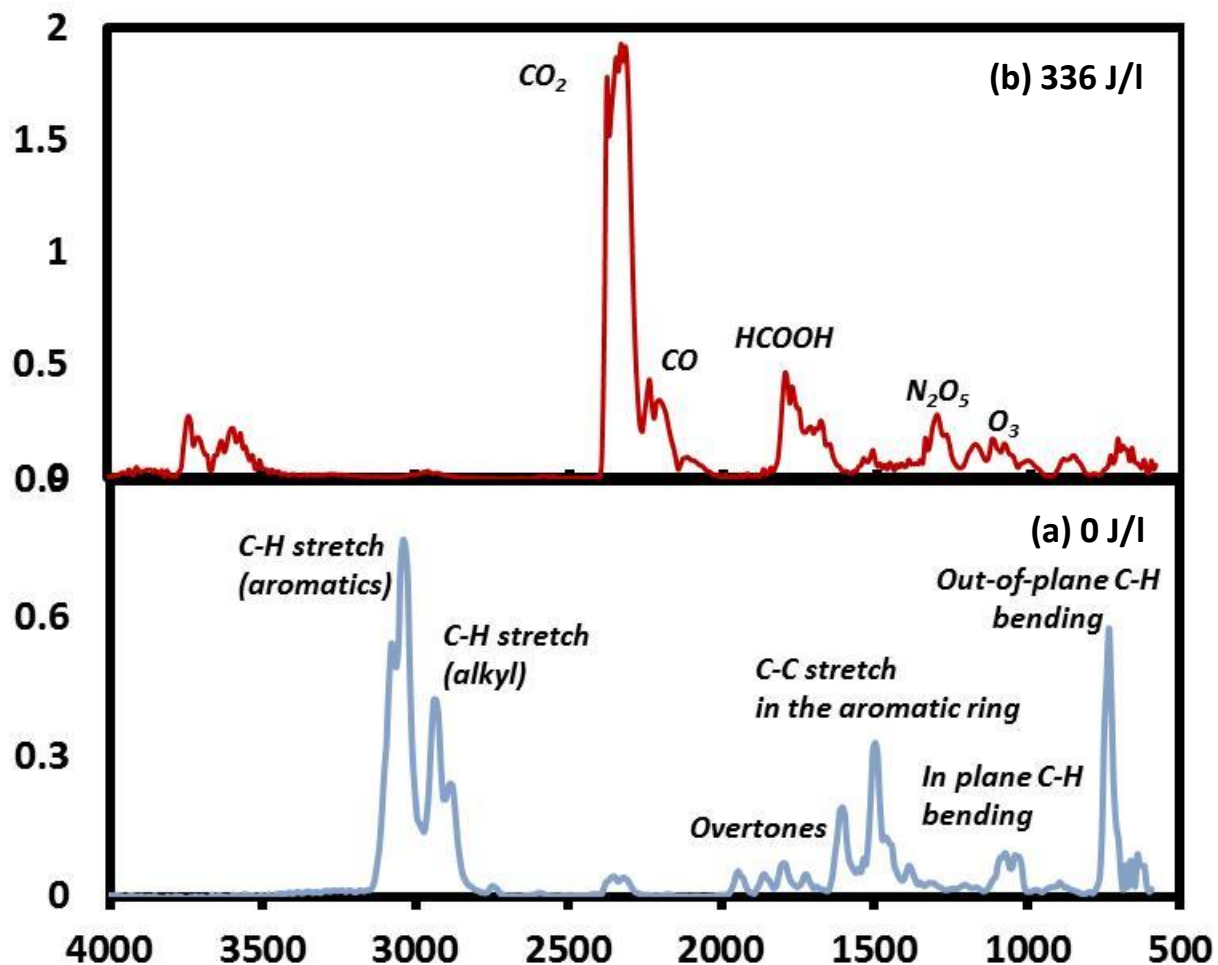




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# FTIR spectra of reaction products in the DBD reactor with TiO<sub>2</sub> catalyst



porosity 2,  
1000 ALD cycles

toluene



Baltic Sea Region  
Programme 2007-2013



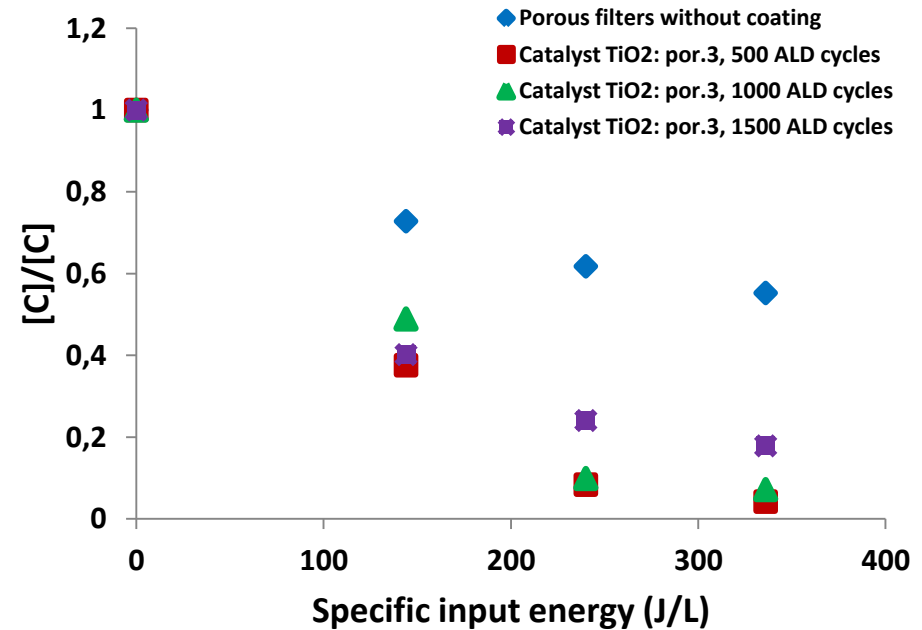
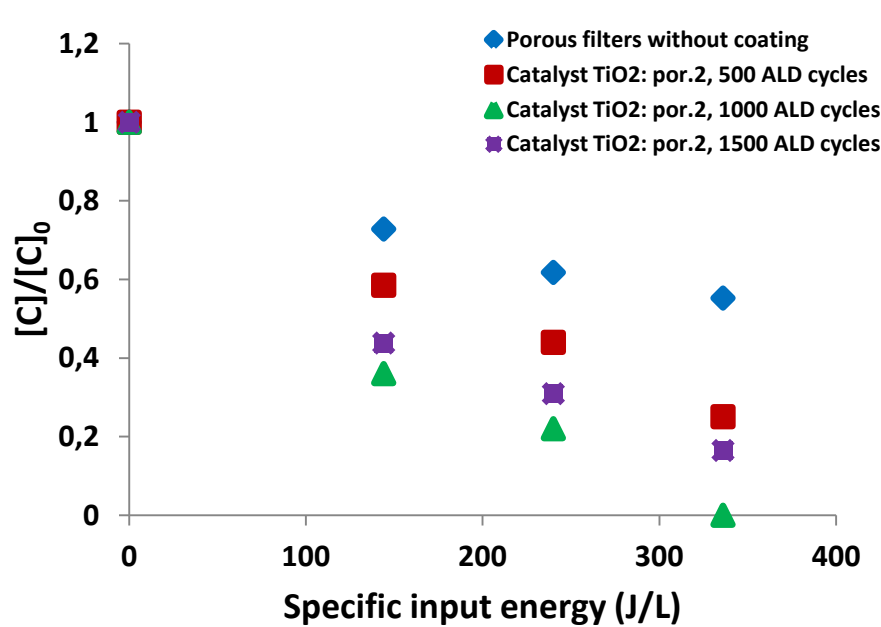
# Effectiveness of catalyst v. SIE



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Relation between the removed amounts of toluene as a function of the specific input energy for different catalyst thickness and pore size



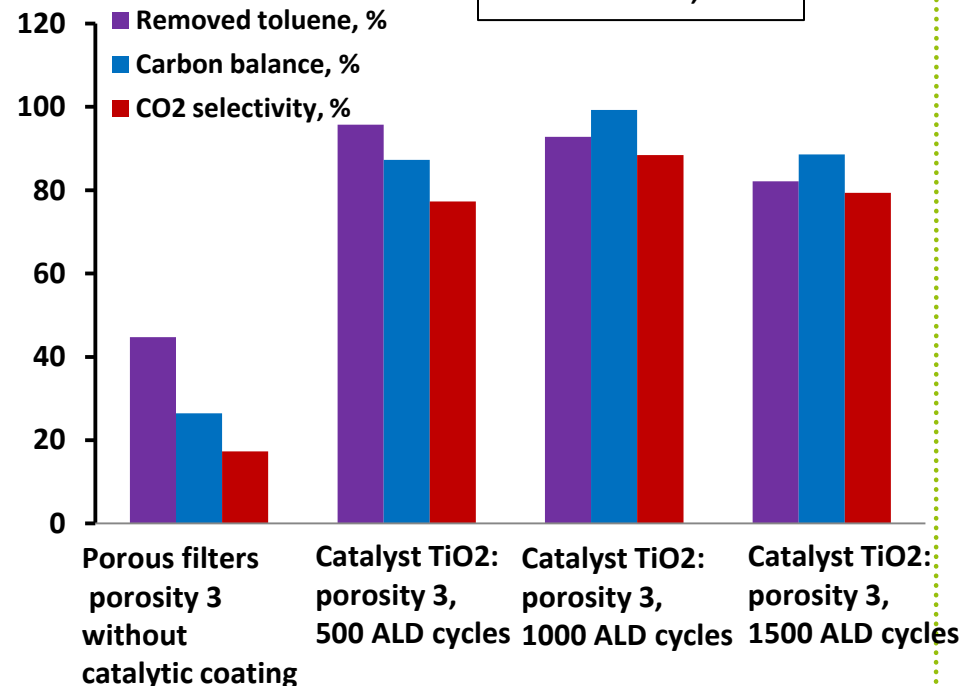
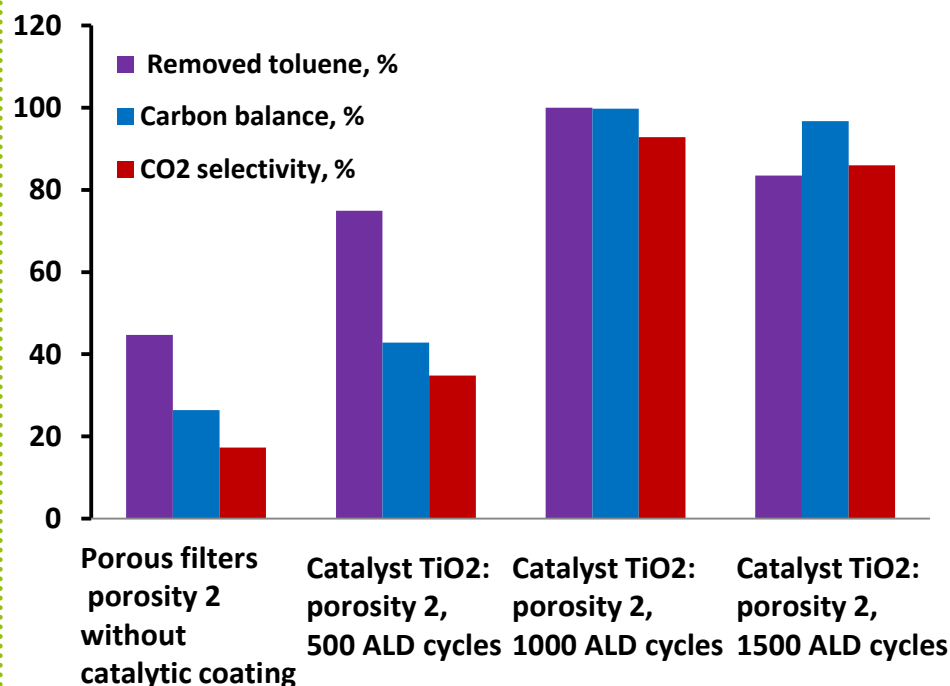


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# Activity of TiO<sub>2</sub> catalysts during the destruction of 2500 ppm of toluene at 336 J/l total gas flow

- Plasma + catalyst removes much more VOCs than plasma alone
- Improves efficiency and selectivity



Best results with ~1000 ALD cycles, approximately 80 nm thick anatase



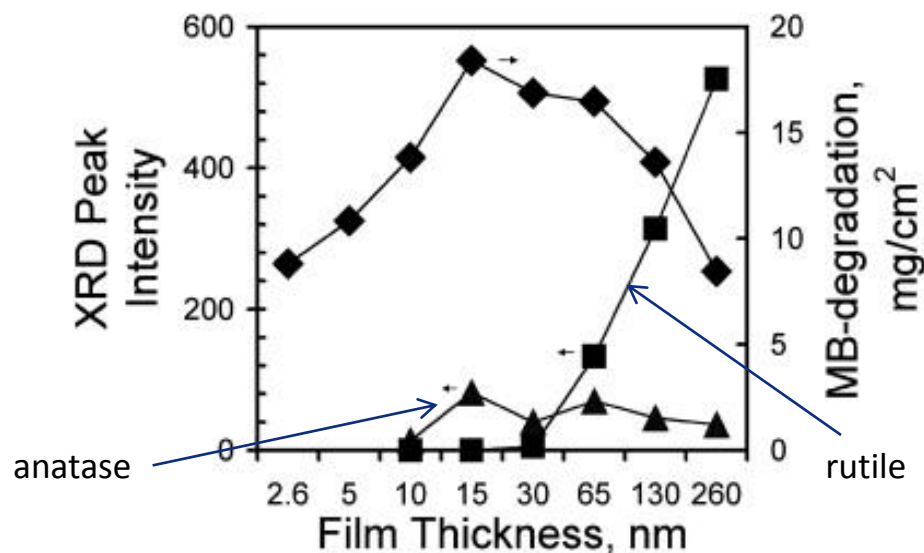


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# Compare with aqueous contamination removal

- Methylene blue in water
- Maximum degradation rate at 15-100 nm film thickness



\* M.-L. Kääriäinen, T.O. Kääriäinen, D.C. Cameron Thin Solid Films Volume 517, Issue 24 2009 6666 – 6670



# Effects of plasma and catalyst together



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- **Photogeneration of electrons and their chemical reactions**
- **Plasma-induced adsorption and desorption of contaminants and by-products**
- **Increased gas residence times by adsorption – more chance of a degradation reaction**
- **Modification of plasma properties by the catalyst**
- **Some local heating of the catalyst by the plasma**
- **Local intensification of the plasma discharge**
- **Modification of the mass transfer properties to the surface of the catalyst**





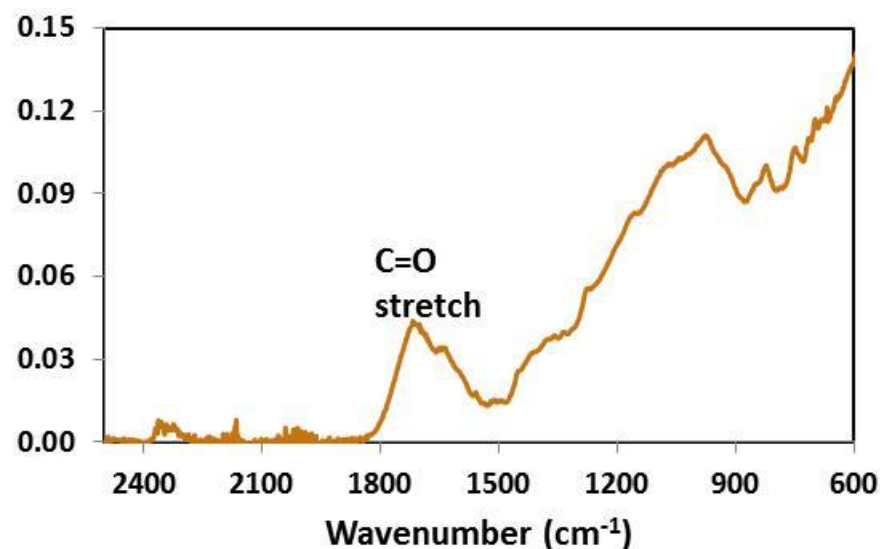
# Contamination



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- Photocatalysts can generate reaction intermediates, which can accumulate on the active sites of the photocatalyst surface, resulting in a decrease in photocatalytic activity with time:
- Identified from FTIR signature
- Benzaldehyde and benzoic acid in toluene oxidation
- Possible periodic removal using oxygen plasma?



# Summary



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- Plasma catalytic reactors using anatase titanium dioxide significantly increase the efficiency of VOC removal over the use of plasma alone.
- Large catalyst area can be achieved by ALD coating of porous materials.
- FTIR spectra show the major reaction products of toluene in the DBD reactor are CO<sub>2</sub> and CO.
- No carbon ring-retaining products were observed after the toluene passed through the DBD reactor with TiO<sub>2</sub> coated catalyst under the correct conditions.
- The efficiency of toluene removal depends on the thickness of the catalyst (optimum ~80 nm) and the porosity of glass filters.





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**Thank you for your attention**

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